Application No.: 10/568,723

Filing Date: February 17, 2006

AMENDMENTS TO THE CLAIMS

 (Previously presented) A method for separating mono-branched hydrocarbons from a mixture of hydrocarbons comprising:

- bringing said mixture into contact with one adsorbent having a selectivity order from mono-branched to linear further to multi-branched hydrocarbons,
- preferentially and selectively adsorbing said mono-branched hydrocarbons by said adsorbent, and
- desorbing said mono-branched hydrocarbons from said adsorbent, thereby selectively separating said mono-branched hydrocarbons.
- (Previously presented) The method according to claim 1 comprising the step of bringing said mixture into contact with only one absorbent.
- 3. (Previously presented) A method for separating mixtures of hydrocarbons into fractions of linear, mono- branched and multi-branched hydrocarbons comprising the steps of:
 - a. bringing said mixture into contact with only one adsorbent, said adsorbent having a selectivity order from mono-branched to linear further to multibranched hydrocarbons,
 - separating a stream enriched in multi-branched hydrocarbons from said adsorbent, thereby separating said multi-branched hydrocarbons,
 - c. desorbing the linear hydrocarbons from said adsorbent, thereby separating said linear hydrocarbons, and
 - d. desorbing said mono-branched hydrocarbons from said adsorbent, thereby separating said mono-branched hydrocarbons.
- 4. (Previously presented) The method according to claim 1, wherein said hydrocarbons are alkanes
- (Previously presented) The method according to claim 1, wherein said adsorbent is a zeolitic adsorbent.

Application No.: 10/568,723

Filing Date: February 17, 2006

6. (Previously presented) The method according to claim 1, wherein said adsorbent is a zeolitic adsorbent having cavities of which the dimensions are larger than the pore openings giving access to said cavities, these cavities having a smallest diameter of at least 4.5 Angström and a largest diameter of at least 10 Angström.

- 7. (Previously presented) The method according to claim 6, wherein said cavities have a smallest diameter between 4.5 and 15 Angström, and a largest diameter between 10 and 25 Angström.
- 8. (Previously presented) The method according to claim 5, wherein said zeolitic adsorbent comprises the molar relationship

wherein n is at least 2, X is a trivalent element and Y is a tetravalent element.

- 9. (Previously presented) The method according to claim 8, wherein n is at least 2, wherein X is selected from the group consisting of aluminum, iron, gallium and boron and wherein Y is silicon.
- 10. (Previously presented) The method according to claim 8, wherein n is at least 10, wherein X is aluminum, and wherein Y is silicon.
- 11. (Previously presented) The method according to claim 5, wherein said zeolitic adsorbent is MCM-22.
- 12. (Previously presented) The method according to claim 5, wherein said zeolitic adsorbent has a pore occupancy comprised between 0.01 and 100%.
- 13. (Previously presented) The method according to claim 4 wherein said mixture of alkanes is a mixture selected from linear, mono-branched and multi-branched alkanes.

Application No.: 10/568,723

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14. (Previously presented) The method according to claim 13, wherein said mixture comprises

0.1-99. 9% linear, 0.1-99. 9% mono-branched and 0.1-90% multi-branched alkanes.

15. (Previously presented) The method according to claim 13, wherein said mixture of alkanes is

a mixture of linear and mono-branched alkanes in a ratio comprised between 1: 100 to 100: 1.

16. (Previously presented) The method according to claim 15, wherein said mixture comprises

mono-branched and linear alkanes in a ratio of 1: 1.

17. (Previously presented) The method according to claim 1, wherein said separation is based on

entropic effects.

18. (Currently amended) A method for separating mono-branched hydrocarbons from a mixture

of hydrocarbons consisting of linear, mono-branched, and multi-branched alkanes which comprises bringing said mixture of hydrocarbons into contact with only one zeolitic adsorbent,

account of the state of the sta

 $\underline{\text{wherein mono-branched alkanes from said mixture are preferentially absorbed}}.$

19-21. (Canceled)

22. (Previously presented) The method according to claim 18, wherein said separation is based

on entropic effects.

23. (Previously presented Currently amended) A method for separating mixtures of non-aromatic

hydrocarbons into fractions of linear, mono-branched and multi-branched hydrocarbons which

comprises contacting said mixture with The method according to claim 18, wherein said one

 $\underline{\text{zeolitic adsorbent is}} \ \text{MCM-22 as a zeolite having a catalytic and an adsorbent activity}.$

-4-